

**INTERNATIONAL JOURNAL OF ENGINEERING SCIENCES & RESEARCH
TECHNOLOGY****MASS TRANSFER KINETICS DURING OSMOTIC DEHYDRATION OF AONLA
SLICES (*Emblica officinalis* Gaertn.) OF Cv. NA-7 PRIOR TO AIR DRYING****M.S. Jadhav*, H.G. More and C.A. Nimbalkar***Associate Professor, Department of Agricultural Process Engineering, Mahatma Phule Krishi
Vidyapeeth, Rahuri, India-413722.Ex. Director of Extension Education, Mahatma Phule Krishi Vidyapeeth, Rahuri, India-413722.
Associate Professor, Department of Agricultural Statistics, Post Graduate Institute, Mahatma Phule Krishi
Vidyapeeth, Rahuri, India-413722.**DOI:** 10.5281/zenodo.49782**ABSTRACT**

Osmotic dehydration of aonla slices of NA-7 variety was carried out in order to remove partial moisture prior to mechanical drying by employing sugar syrup solution (50, 60 and 70°Brix) at sugar syrup temperatures (40, 50 and 60°C) and immersion time (15, 30, 60, 90, 120, 180 and 240 min) maintaining constant solution to fruit ratio of 6:1 (v/w). The effects of syrup concentration, syrup temperature and immersion time on water loss and sugar gain were observed. It was found that water loss and sugar gain both were increased non-linearly with syrup concentration, temperature and immersion time and found in the range of 13.60 to 59.52 and 2.53 to 17.10 %, respectively. Among the seven existing mathematical models tried, the logarithmic model was found adequate to describe the water loss for all the temperature-concentration combinations except treatment of 60°C-70°B for which power model was found adequate based on regression diagnostic criteria. For sugar gain, the quadratic model for 40°C-50 °B, cubic model for 40°C-50 and 70°B, 50°C-50 and 70°B and for 60°C-50°B noticed best fit however, the logarithmic model was found best for 50°C-60°B, 60°C-50 and 60°B temperature-concentration combinations. The developed models can be used for predicting water loss and sugar gain during osmotic dehydration of aonla slices within the range of experimental study.

KEYWORDS: Aonla, Osmotic dehydration, Modelling, Water loss, Sugar gain.**INTRODUCTION**

Osmotic dehydration (OD) of food got attention due to its importance in food processing industries. OD is a process for the partial removal of water from plant tissues such as fruits and vegetables by immersion in an aqueous concentrated solution of soluble salts. A driving force for the diffusion of water from the tissue into the solution is provided by the difference in osmotic pressure or concentration gradient between the food and surrounding osmotic solution. A diffusion of water is accompanied by the simultaneous counter diffusion of solute from the osmotic solution into the tissue. Since the membrane responsible for the osmotic transport is not perfectly selective, other solutes such as sugar, organic acids, minerals, salts and vitamins present in the cells can also be leached into the osmotic solution (Giangiacomo *et al.* [6] and Tortoe *et al.* [19]). But this flow can be quantitatively neglected. Kinetics of dewatering and mass transfer have been investigated for banana (Pokharkar and Prasad [14]); melons (Rodrigues and Fernandes[17]); apple, banana and potato (Tortoe *et al.* [20]) and papaya (Jain *et al.* [8]). India is the largest producer of fruits like mango, banana, papaya, sapota, pomegranate and aonla. In India, area under aonla was about 1,03,550 ha with production of about 12,25,210 metric tonnes during the year 2013-14

(Anonymous [2]). Aonla is known for exceptionally high amount of ascorbic acid and is regarded by the Indian scientist as richest and cheapest source of vitamin-C. It contains 600-900 mg of ascorbic acid per 100 g of pulp. The pulp contains protein (0.05%), phosphorus (0.2%), iron (1-2%) and nicotinic acid (0.2 mg/100 g) with a high amount of pectin (Pokharkar [15]). The rate of mass transfer (water loss and sugar gain) was found to be a function of many variables such as solution temperature, solution concentration, composition of osmotic solution, immersion time, nature of food and its geometry, solution to fruit ratio. Keeping in view, the perishable nature of aonla fruits, the objective of the present study was to investigate the effect of osmotic process parameters on mass transfer kinetics of aonla slices and to develop the mathematical models for water loss and sugar gain.

MATERIALS AND METHODS

Fresh aonla fruits of variety NA-7 (*Neelam*) were procured from an orchard of Department of Horticulture, Mahatma Phule Krishi Vidyapeeth, Rahuri (India). The aonla fruits were sorted for uniform size (32.5 ± 1 mm), colour, maturity and physical damage; washed with potable water and then wiped with a muslin cloth to remove surface moisture. Fruits were blanched in boiling water for 5 min and cut to 5 mm thick uniform slices with specially designed radial type aonla cutter. Cut slices were separated with a sharp stainless steel knife and held in water until the entire batch was prepared to prevent enzymatic browning. Slices were then removed from the water and gently blotted with tissue paper prior to osmotic drying and determination of moisture content. Moisture content of the fresh as well as osmotically dehydrated aonla slices were determined by vacuum oven method. A pre weighed 3-5 g sample of aonla slices was kept in pre-dried and weighed petri-dishes. The petri-dishes with samples were placed in vacuum oven at 70°C maintaining vacuum between 85 to 100 mm of Hg till it attained constant weight. Petri-dishes were then cooled in desiccators for one hour and weighed. Average moisture content of three replicated samples was recorded (Ranganna [16]).

Preparation of sugar syrup as osmotic agent

Sugar syrups of three concentrations (50, 60 and 70°B) were prepared by dissolving known quantity of sugar in distilled water using glass rod as stirrer. Concentration of sugar syrup was checked by using hand refractometer (Erma Japan make) of appropriate range (0-32, 28-62 and 58-92 $^{\circ}\text{B}$). Sugar was procured from local market and used as osmotic agent as it prevents food discolouration to a large extent and imparts good taste to the final product.

Experimental procedure

In osmotic dehydration, a sample of aonla slices of 5 mm thickness each weighing 75 g were prepared. Constant syrup to fruit ratio (STFR) of 6:1 (v/w) was used. The 500 mL capacity glass beakers containing sugar syrup (50, 60 and 70°B) were placed inside the constant temperature circulatory water bath (Make: Classic Scientific India, Thane) at (40, 50 and 60°C) and slices were put into the syrup after attainment of desired temperature. Sodium metabisulphite (0.1%) was added to each beaker containing the syrup. For every 15, 30, 60, 90, 120, 180 and 240 min interval one glass beaker was removed from the water bath and the aonla slices were immediately rinsed with distilled water to remove the solute adhered to fruit surface. Then slices were spread on the tissue paper for 5 min to remove the surface moisture. The weight of osmotically dehydrated aonla slices was recorded. Slices were then put in pre-weighed petri-dish for moisture determination by vacuum oven method. Each treatment replicated thrice and average moisture content was recorded.

Osmotic dehydration parameters

Lenart and Flink [11] first defined terminology for mass transport data which helped to study the characteristics of osmosis process during dehydration of product and same had been used by Kaleemullah *et al.* [9].

Water loss

Water loss is the quantity of water lost by food during osmotic processing. The water loss (WL) is defined as the net weight loss of the fruit on initial weight basis and was estimated as :

$$WL = \frac{W_i X_i - W_0 X_0}{W_i} \times 100 \quad \dots (1)$$

where,

WL = Water loss (% or g per 100 g mass of sample).

W_0 = Mass of slices after time θ , g

W_i = Initial mass of slices, g

X_0 = Water content as a fraction of mass of slices at time, θ

X_i = Water content as a fraction of initial mass of slices, fraction

Sugar gain

Sugar molecules from the osmotic solution get diffused to the sample of aonla slices during osmotic dehydration. The loss of water from the sample takes place in osmotic dehydration consequently, it increases the sugar content. Sugar gain is the net uptake of sugar by the slices on initial weight basis. It will be computed using following expression:

$$SG = \frac{W_0(1-X_0)-W_i(1-X_i)}{W_i} \times 100 \quad \dots (2)$$

where,

SG = Sugar gain (% or g per 100 g mass of sample).

W_0 = Mass of slices after time θ , g

W_i = Initial mass of slices, g

X_0 = Water content as a fraction of mass of slices at time θ .

X_i = Water content as a fraction of initial mass of slices, fraction.

Modelling of mass transport kinetics

Water loss and sugar gain were plotted as ordinate against time of osmosis as abscissa and mathematical models for dependent variable Y (WL and SG) and independent variable t (time of osmosis) given in Table 1 were developed by regression analysis. Model constants a, b, and c were determined. Statistical package SAS 9.3 was used for analysis of data.

Validation of model for osmotic mass transfer kinetics

In order to validate the model and check the goodness of fit on the basis of highest coefficient of determination (R^2), highest adjusted coefficient of determination (Adj. R^2), lowest chi-square statistic, probability, root mean square error (RMSE), mean bias error (MBE) and per cent error modulus between experimental and predicted values were considered and evaluated by performing regression analysis as follows.

$$R^2 = 1 - \left[\frac{SS_{\text{residual}}}{SS_{\text{model}} + SS_{\text{residual}}} \right] \quad \dots (3)$$

$$\begin{aligned} \text{Adjusted } R^2 &= 1 - \left[\frac{SS_{\text{residual}}/(n-p)}{(SS_{\text{model}} + SS_{\text{residual}})/(n-1)} \right] \\ &= 1 - \left[\frac{(n-1)}{(n-p)} \right] (1 - R^2) \quad \dots (4) \end{aligned}$$

$$\chi^2 = \left[\sum_{i=1}^n \frac{(V_{\text{expt.}} - V_{\text{pred.}})^2}{\text{pred.}} \right] \quad \dots (5)$$

$$RMSE = \frac{1}{n} \left[\sum_{i=1}^n (V_{\text{expt.}} - V_{\text{pred.}})^2 \right]^{0.5} \quad \dots (6)$$

$$\text{Mean Bias Error} = \frac{1}{n} \sum_{i=1}^n (V_{\text{expt.}} - V_{\text{pred.}}) \quad \dots (7)$$

$$\text{Per cent Error Modulus} = \frac{100}{n} \left| \sum_{i=1}^n \frac{(V_{\text{expt.}} - V_{\text{pred.}})}{V_{\text{pred.}}} \right| \quad \dots (8)$$

where,

$V_{\text{expt.}}$ = Experimental value of WL or SG (%)

$V_{\text{pred.}}$ = Predicted value WL or SG (%)

n = Number of observations

p = Number of variables

RESULTS AND DISCUSSION

Effect of osmotic dehydration process parameters on water loss

Average initial moisture content of fresh aonla fruits of variety NA-7 was found 86.101 (% w. b.).

Data of water loss as influenced by various sugar syrup concentrations (50, 60 and 70°B), sugar syrup temperatures (40, 50 and 60°C) and immersion time (15, 30, 60, 90, 120, 180 and 240 min) during osmotic dehydration of aonla slices is presented in Table 2 and same is plotted in Fig. 1.

It is observed from Fig. 1 that the water loss was very fast at the beginning of the process and rate was gradually decreased with the increase of immersion time for all the treatment combinations. It can be further seen that as the immersion time increased the water loss was increased; however the equilibrium point could not be reached after short duration (4 h) of the osmotic dehydration process. This result is in confirmation with Lenart and Flink [11]; Jain *et al.* [8] and Alam and Singh [1].

When sugar syrup temperature was increased from 40 to 50°C for 70°B syrup concentration, the water loss increased from 48.56 to 53.44 per cent after 4 h of osmotic dehydration causing 4.88 per cent point increase, however further increase in syrup temperature to 60°C, the water loss was 59.52% showing 6.08% point increase. Similarly for 60°B syrup concentration, the water loss was increased from 46.32 to 50.44 per cent when syrup temperature increased from 40°C to 50°C giving only 4.12 per cent point gain and further increase in syrup temperature from 50 to 60°C, the water loss was increased to 54.02% showing 3.58 per cent point increase. Similar results were obtained for 50°B sugar syrup concentration with the corresponding increase of 2.47 per cent point when sugar syrup temperature was increased from 40°C to 50°C and 4.48 per cent point when temperature was increased from 50 to 60°C. Water loss was in the range of 13.60 to 59.52 per cent. A low temperature-low concentration (40°C-50°B) gave a low water loss (44.04% after 4 h of osmosis) and a high temperature-high concentration conditions (60°C-70°B) gave a higher water loss (59.52% after 4 h of osmosis). Low temperature-high concentration condition 40°C-70°B gave a slightly lower water loss of 48.56% after 4 h of osmosis than 60°C- 50°B (50.99% after 4 h of osmosis) indicating a slightly greater temperature effect on water loss (Table 2). This indicated that water loss can be increased by either increasing the sugar syrup temperature or concentration of solution. However, an increase in temperature of sugar solution by 20°C has more influence on water loss than increase in concentration by 20°B. Similar results were obtained by Videv *et al.* [21] for osmotic dehydration of apples and Jain *et al.* [8] for osmotic dehydration papaya cubes.

Water loss at any concentrations was affected by the temperature of sugar syrup. It was increased non-linearly with increase in syrup temperature and then the rate decreased. This may be due to changes in semi-permeability of the cell membrane of the fruit, allowing more water to diffuse out in shorter period. Similar results were obtained by Conway *et al.* [4] for osmotic dehydration of apples and Kar and Gupta [10] for air drying of osmo-dehydrated mushrooms. At higher temperature, the viscosity of syrup may be decreased, causing setting of convection currents in the syrup, which in turn eliminated local dilution and favoured osmosis. Similar trends were observed by Jain *et al.* [8] for osmotic dehydration kinetics of papaya cubes.

Water loss was very fast at the beginning of process and rate decreased gradually with the increase of duration of osmosis, but did not approach the equilibrium (Fig.1). Similar results were quoted in case of the osmotic dehydration of green beans by Biswal *et al.* [3] and for banana slices by Pokharkar and Prasad [14]. It was also observed that the water loss increased with increase in syrup concentration also at a particular temperature of syrup. This may be due to increased osmotic pressure in the sugar syrup at higher concentrations, which might have increased the driving force available for water transport. Similar findings were observed by Parjoko *et al.* [13] for osmotic dehydration kinetics of pineapple and Magee *et al.* [12] for apple slices.

Effect of osmotic dehydration process parameters on sugar gain

Data of sugar gain as affected by various sugar syrup concentrations (50, 60 and 70°B), temperatures (40, 50 and 60°C) and immersion time (15, 30, 60, 90, 120, 180 and 240 min) during osmotic dehydration of aonla slices is depicted in Table 3 and same is plotted in Fig 2.

It is evident from Fig 2 that the sugar gain was very fast during the first hour of the process and rate was gradually decreased with the increase of immersion time. It can be further seen that as the immersion time increased the sugar gain was increased; however the equilibrium point could not be reached after short duration (4 h) of the osmotic dehydration process. This result is in confirmation with Jain *et al.* [8] and Alam and Singh [1].

When sugar syrup temperature was increased from 40 to 50°C for 70°B syrup concentration, sugar gain increased from 14.51 to 16.05 per cent after 4 h of osmotic dehydration causing 1.54 per cent point increase, however further increase in syrup temperature to 60°C, the sugar gain was 17.10% showing 1.05% point increase. Similarly for 60°B syrup concentration, the sugar gain was increased from 12.72 to 13.22 per cent when syrup temperature increased from 40°C to 50°C giving only 0.50 per cent point gain and further increase in syrup temperature from 50 to 60°C, the sugar gain was increased to 14.17% showing 0.95 per cent point increase. Similar results were obtained for 50°B sugar syrup concentration also with the corresponding increase of 1.38 per cent point when sugar syrup temperature was increased from 40 to 50°C and 0.32 per cent point when temperature was increased from 50 to 60°C. The sugar gain was in the range of 2.53 to 17.10 per cent. A low temperature-low concentration (40°C-50°B) gave a low sugar gain (11.15% after 4 h of osmosis) and a high temperature-high concentration conditions (60°C-70°B) gave a higher sugar gain (17.10% after 4 h of osmosis). Low temperature-high concentration condition 40°C-70°B gave a slightly higher sugar gain of 14.51% after 4 h of osmosis than 60°C- 50°B (12.85% after 4 h of osmosis) indicating a slightly lower temperature effect on sugar gain which may be due to structural composition of a particular variety (Table 3). This indicates that sugar gain can be increased by either increasing the sugar syrup temperature or concentration of solution. However, an increase in temperature of sugar solution by 20°C has more influence on sugar gain than increase in concentration by 20°B. Similar results were obtained by Videv *et al.* [21] for osmotic dehydration of apples and Jain *et al.* [8] for papaya cubes.

Sugar gain at any concentrations was affected by the temperature of sugar syrup. It was increased non-linearly with increase in syrup temperature and then the rate decreased. This may be due to rapid sugar uptake near the surface in the beginning might have resulted in structural changes leading to compaction of these surface layers and increased mass transfer resistance for sugar uptake (Lenart and Flink [11]). Similar trends have been reported for other fruits and vegetables during osmosis by Sutar and Gupta [18] and Ertekin and Cakaloz [5].

It is further observed from Fig. 2 that, the sugar gain was very fast at the beginning of process and rate decreased gradually with the increase of duration of osmosis, but did not approach the equilibrium for both the varieties. The similar results were quoted in case of the osmotic dehydration of green beans by Biswal *et al.* [3] and for banana slices by Pokharkar and Prasad [14]. It was also observed that the sugar gain increased with increase in syrup concentration also at a particular temperature of syrup. This may be due to increased osmotic pressure in the sugar syrup at higher concentrations, which might have increased the driving force available for sugar transport. Sugar gain was also increased with increase in syrup temperature which may be due to the collapse of cell membrane at higher temperatures. Similar findings were observed by Parjoko *et al.* [13] for osmotic dehydration kinetics of pineapple and Magee *et al.* [12] for apple slices.

Modelling of water loss and sugar gain

Among the seven existing models *viz.*, linear, quadratic, cubic, exponential, power and logarithmic tried to fit the experimental data of water loss and sugar gain, the best fit equations and regression diagnostic criteria are presented Table 4 and 5, respectively.

Logarithmic model was found adequate to describe the water loss for all the temperature- concentration combinations except treatment of 60°C-70°B for which power model was found adequate based on regression diagnostic criteria. Per cent error modulus of less than 0.5% also indicated best fit (Table 4).

It is clear that for sugar gain, the quadratic model for 40°C-50°B, cubic model for 40°C-50 and 70°B, 50°C-50 and 70°B and for 60°C- 50°B noticed best fit, whereas, logarithmic model was found best for 50°C-60°B, 60°C-50 and 60°B temperature-concentration combinations based on regression diagnostic criteria (Table 5).

Several researchers modelled the mass transport data of water loss and sugar gain for various fruits and vegetables. Jain *et al.* [7] and Pokharkar and Prasad [14] developed the mathematical models for water loss and sugar gain for papaya cubes and banana slices, respectively.

Table 1 Mathematical models for osmotic dehydration kinetics

Model	Equation
Linear	$Y = a + b t$
Quadratic	$Y = a + b t + ct^2$
Cubic	$Y = a + b t + ct^2 + dt^3$
Exponential	$Y = a e^{bt}$
Power	$Y = a t^b$
Logarithmic	$Y = a + b e^t$

Table 2 Effect of immersion time, temperature and sugar concentration on water loss (%) at 6:1 STFR during osmotic dehydration of aonla slices

Time (min)	40°C			50°C			60°C		
	50°B	60°B	70°B	50°B	60°B	70°B	50°B	60°B	70°B
15	13.60	17.22	19.96	17.15	18.77	25.31	21.29	23.37	34.03
30	23.95	25.94	27.25	28.80	29.84	32.46	29.93	33.92	40.93
60	29.02	32.01	34.98	33.46	34.40	38.71	35.78	38.80	43.10
90	31.85	35.69	38.14	36.77	37.52	42.61	40.11	44.85	49.42
120	35.71	39.06	41.97	39.72	40.72	45.63	43.71	47.72	52.90
180	40.65	42.22	45.54	43.90	45.66	51.51	48.56	50.66	56.25
240	44.04	46.32	48.56	46.51	50.44	53.44	50.99	54.02	59.52

Table 3 Effect of immersion time, temperature and sugar concentration on sugar Gain (%) at 6 : 1 STFR during osmotic dehydration of aonla slices

Time (min)	40°C			50°C			60°C		
	50°B	60°B	70°B	50°B	60°B	70°B	50°B	60°B	70°B
15	2.53	3.98	4.99	5.13	5.30	6.16	6.58	7.56	9.32
30	3.82	5.36	6.57	6.66	7.24	8.52	7.18	9.01	11.59
60	5.75	8.48	11.07	8.72	9.14	12.73	9.28	9.49	13.32
90	6.71	10.42	12.84	9.96	10.67	14.81	10.24	11.37	14.91
120	8.86	11.25	13.23	10.35	11.34	15.33	10.47	11.98	15.37
180	10.25	11.66	14.07	11.23	12.30	15.90	11.51	13.05	16.18
240	11.15	12.72	14.51	12.53	13.22	16.05	12.85	14.17	17.10

Table 4 Best fit models and statistical diagnostic parameters for water loss during osmotic dehydration of aonla slices

Temp. (°C)	Conc. (°B)	Model	Prediction equation	R ²	Adj R ²	Prob	χ ²	RMSE	MBE	% Error Modulus
40	50	Logarithmic	WL = -13.5864 + 10.406638 ln(t)	0.987	0.985	0	0.352	1.278	6E-15	0.3500
	60	Logarithmic	WL = -9.4201 + 10.091281 ln(t)	0.996	0.995	0	0.091	0.701	8E-15	0.1343
	70	Logarithmic	WL = -7.7377 + 10.295632 ln(t)	0.999	0.998	0	0.022	0.396	6E-15	0.0414
50	50	Logarithmic	WL = -7.8735 + 9.992412 ln(t)	0.980	0.976	0	0.507	1.542	6E-15	0.5557
	60	Logarithmic	WL = -8.5388 + 10.51299 ln(t)	0.980	0.976	0	0.429	1.608	-5E-16	0.2629
	70	Logarithmic	WL = -2.6114 + 10.209234 ln(t)	0.996	0.995	0	0.058	0.721	8E-15	0.0271
60	50	Logarithmic	WL = -7.2081 + 10.635698 ln(t)	0.997	0.997	0	0.058	0.620	9E-15	0.0300
	60	Logarithmic	WL = -4.3823 + 10.741842 ln(t)	0.989	0.987	0	0.228	1.229	9E-15	0.2100
	70	Power	WL = 20.069 t ^{0.19868}	0.982	0.978	0	0.001	0.029	1E-16	0.0000

Table 5 Best fit models and statistical diagnostic parameters for sugar gain during osmotic dehydration of aonla slices

Temp (°C)	Conc. (°B)	Model	Prediction equation	R ²	Adj R ²	Prob	χ ²	RMSE	MBE	% Error Modulus
40	50	Quadratic	SG= 1.5173 + 0.0776t- 0.0002 t ²	0.996	0.994	0	0.038	0.252	4E-16	0.2329
	60	Cubic	SG= 1.412 + 0.169 t-0.001 t ² + 0 t ³	0.997	0.994	3E-04	0.037	0.259	9E-16	0.0843
	70	Cubic	SG= 1.804 + 0.213 t-0.0012 t ² + 0 t ³	0.991	0.981	0.002	0.095	0.52	-2E-15	0.0643
50	50	Cubic	SG= 3.45 + 0.127 t-0.0008 t ² + 0 t ³	0.999	0.997	1E-04	0.006	0.14	-1E-15	0.0257
	60	Logarithmic	SG= -2.4636 + 2.865924 ln(t)	0.998	0.998	0	0.009	0.14	3E-15	0.0257
	70	Cubic	SG= 2.92 + 0.232 t - 0.0014 t ² + 0 t ³	0.997	0.995	2E-04	0.019	0.289	-1E-15	0.0043
60	50	Cubic	SG= 5.116 + 0.095 t- 0.0005 t ² + 0 t ³	0.992	0.984	0.001	0.029	0.283	1E-15	0.0429
	60	Logarithmic	SG= 0.4996 + 2.440738 ln(t)	0.994	0.993	0	0.017	0.201	-5E-16	0.0086
	70	Logarithmic	SG= 2.0292 + 2.771019 ln(t)	0.993	0.992	0	0.023	0.251	2E-15	0.0614

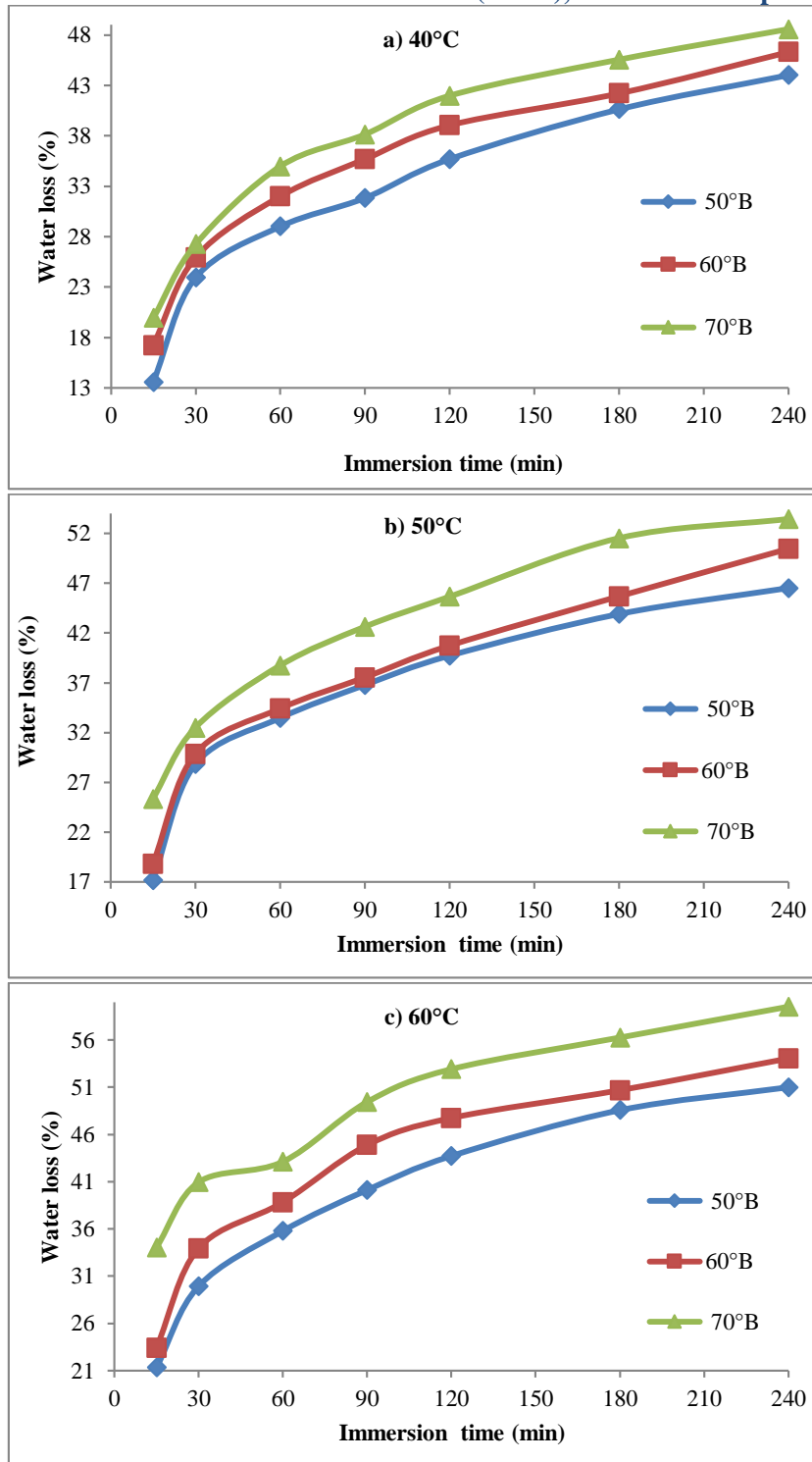


Fig. 1 Effect of immersion time and sugar concentration on water loss (%) at 6:1 STFR during osmotic dehydration of aonla slices at a) 40; b) 50 and c) 60°C

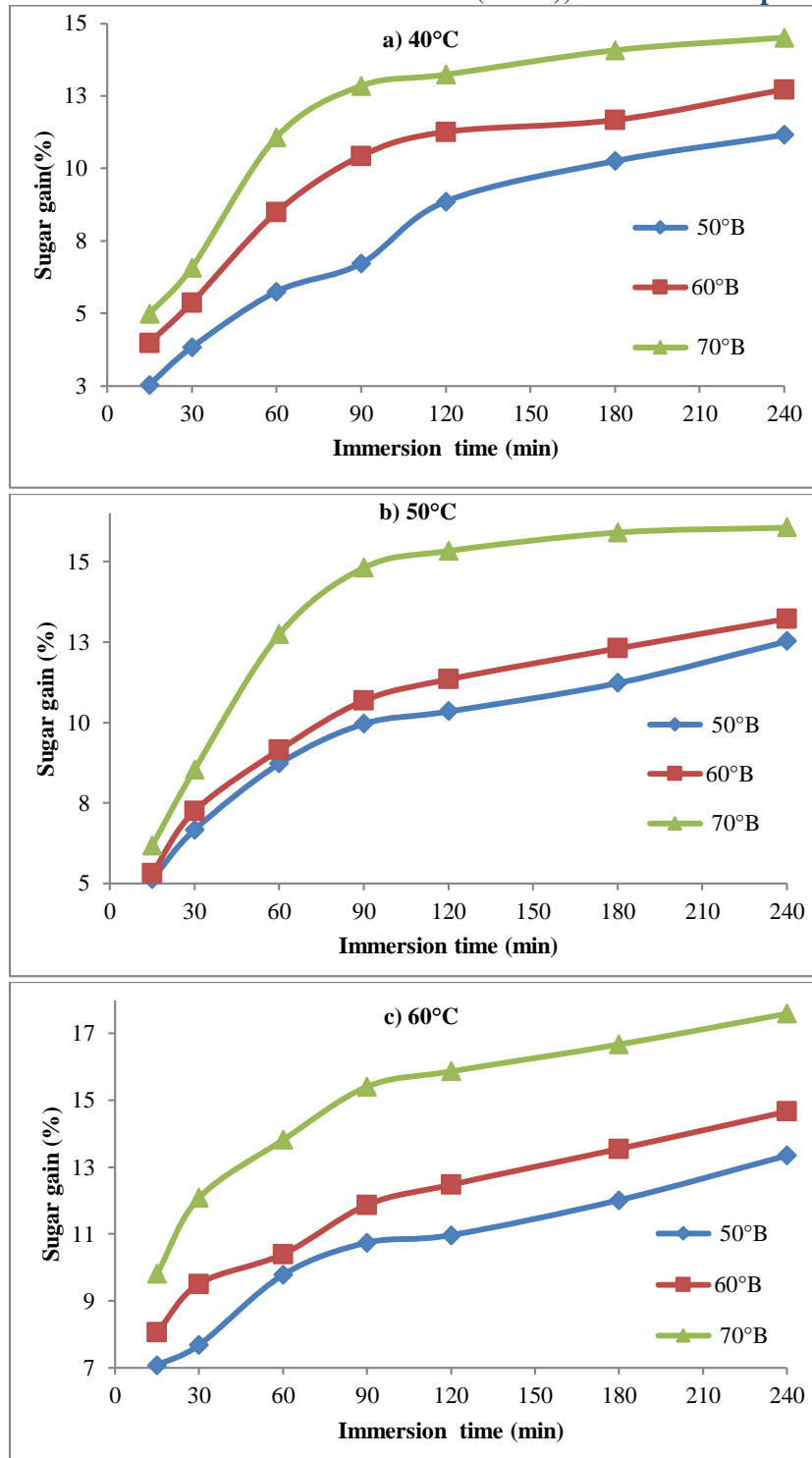


Fig. 2 Effect of immersion time and sugar concentration on sugar gain (%) at 6:1 STFR during osmotic dehydration of aonla slices at a) 40; b) 50 and c) 60°C

CONCLUSION

Aonla slices can be partially dewatered by osmotic dehydration in sugar solution. They can lose 13.60 to 59.52 % water and gain 2.53 to 17.10 % sugar depending upon the sugar syrup concentration (50-70°Brix) and temperature (40-60°C) in 4 h duration of osmosis. Water loss and sugar gain by aonla slices during osmotic dehydration in different sugar syrup concentration and temperature were modelled. Models will be useful to know the osmotic dehydration time in getting the desired level of sugar gain in aonla slices. These developed models could be used in food industry for design and control process.

REFERENCES

- [1] Alam, M.S. and A. Singh. 2008. Modelling of mass transfer in osmotic dehydration of aonla slices. *Journal of Agricultural Engineering*, 45(3): 38-44.
- [2] Anonymous. 2014. Indian Horticulture Database-2014, National Horticultural Board, Ministry of Agriculture. Govt. of India.
- [3] Biswal, R.N., K. Bozorgmehr., F.D. Tompkins and X. Liu. 1991. Osmotic concentration of green beans prior to freezing. *Journal of Food Science*, 56: 1008-1012.
- [4] Conway, J., F. Castaigne., G. Picard and X. Venan. 1983. Mass transfer consideration in the osmotic dehydration of apples. *Canadian Institute of Food Science and Technology Journal*, 16: 25-29.
- [5] Ertekin, F.K. and T. Cakoloz. 1996. Osmotic dehydration of peas: I. Influence of process variables on mass transfer. *Journal of Food processing and Preservation*, 20: 87-95.
- [6] Giangiacomo, R., D. Torreggiani and E. Abbo. 1987. Osmotic dehydration of fruit. Part I :Sugar exchange between fruit and extracting syrup. *Journal of Food processing and Preservation*, 11: 183-195.
- [7] Jain, S.K., R.C. Verma and A.N. Mathur. 2003. Osmo-convective drying of papaya. *Beverage and Food World*, 30(1): 64-67.
- [8] Jain, S.K., R.C. Verma., L.K. Murdia and H.K. Dashora. 2011. Optimisation of process parameters for osmotic dehydration of papaya cubes. *Journal of Food Science and Technology*, 48(2): 211-217.
- [9] Kaleemullah, S., R. Kallippan and N. Varadhrāju. 2002. Studies on osmotic air drying characteristics of papaya cubes. *Journal of Food Science and Technology*, 39(1): 82-84.
- [10] Kar, A. and D.K. Gupta. 2001. Osmotic dehydration characteristics of button mushrooms. *Journal of Food Science and Technology*, 38(4): 352-357.
- [11] Lenart, A. and J.M. Flink. 1984. Osmotic concentration of potato. I. Criteria for end point of the osmosis process *Journal of Food Engineering*, 19: 45-63.
- [12] Magee, T.R.A., A.A. Hassaballah and W.R. Murphy. 1983. Internal mass transfer during osmotic of apple slices in sugar solution. *Journal of Food Science and Technology*, 7(1): 147-155.
- [13] Parjoko, M., S. Rahman., K.A. Buckle and C.O. Perera. 1996. Osmotic dehydration kinetics of pineapple wedges using palm sugar. *Lebensmittel Wissenschaft and Technologie, International Journal of Food Science and Technology*, 29(5-6): 452-459.
- [14] Pokharkar, S.M. and S. Prasad. 1998. Mass transfer during osmotic dehydration of banana slices. *Journal of Food Science and Technology*, 30(4): 336-338.
- [15] Pokharkar, S.M. 2005. Development and performance evaluation of aonla shredding machine. *Beverage and Food World*, 32(3): 52-53.
- [16] Ranganna, S. 2005. *Handbook of Analysis and Quality Control for Fruits and Vegetable Products*. Tata McGraw Hill Publishing Co. Ltd., New Delhi.
- [17] Rodrigues, S. and F.A.N. Fernandes. 2007. Dehydration of melons in a ternary system followed by air drying. *Journal of Food Engineering*, 80: 678-687.
- [18] Sutar, P.P. and D.K. Gupta. 2007. Mathematical modelling of mass transfer in osmotic dehydration of onion slices. *Journal of Food Engineering*, 78: 90-97.
- [19] Tortoe, C., J. Orchard and A. Beezer. 2007. Comparative behaviour of cellulosic and starchy plant materials during osmotic dehydration *Journal of the Science Food and Agriculture*, 87: 1284-1291.
- [20] Tortoe, C., J. Orchard and A. Beezer. 2011. Multilinear regression approach in predicting osmotic dehydration process of apple, banana and potato. *Journal of Food Processing Technology*, 2:122. doi: 10.4172/2157-7110.1000122.

- [21] Videv, K., T. Tanchev., R.C. Sharma and V.K. Joshi. 1990. Effect of sugar syrup concentration and temperature on the rate of osmotic dehydration of apples. *Journal of Food Science and Technology*, 27(5): 307-308.